

# Combustion and Detonation Control by in-Situ Blending of Liquid Fuels

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Jet propulsion kerosene and hydrogen peroxide are the promising compounds for applications in advanced propulsion systems. Flammability and detonability of sprays and vapors of kerosene and hydrogen peroxide were shown to differ essentially. When mixed with air together and in proper amounts, they can be readily detonated by a relatively weak ignition source. Hybrid combustion of hydrocarbon and hydrogen peroxide droplets has been studied in detail.

## 1. Introduction

The operational ability of air-breathing propulsion engines (both in deflagration and detonation modes) is considerably dependent on the fuel used. One of the promising solutions to actively control combustion or detonation is to inject several liquid fuels into a combustion chamber. The study particularly implies the use of two liquid fuels: conventional kerosene and hydrogen peroxide. Detailed description of hydrogen peroxide applications in various types of propulsion devices can be found elsewhere [1–3].

The main objective of the research was to analyze the reactivity and performance stability of the fuel blends in terms of the critical initiation energy of detonation, combustion and detonation parameters and their sensitivity to ambient conditions, specific impulse, ignition delay, and combustion of droplets.

## 2. Previous Accomplishments

Flammability and detonability of air mixtures (both gas-phase and heterogeneous) of hydrocarbon fuels (*n*-heptane, *iso*-octane, and *n*-tetradecane) with hydrogen peroxide was studied theoretically in [4–7]. According to [8], the listed hydrocarbons approximately represent jet propulsion kerosene (It is known that kerosene can be considered to be made up of approximately 79% high *n*-alkanes, 10% cycloalkanes and 11% aromatics). The following results have been obtained:

(1) The flame velocity in suspensions of *n*-heptane droplets in air with addition of H<sub>2</sub>O<sub>2</sub> vapor increases with the concentration of H<sub>2</sub>O<sub>2</sub> vapor in the mixture, in spite of the fact that the initial concentration of oxygen in the mixture decreases. Addition of H<sub>2</sub>O<sub>2</sub> vapor to kerosene–air mixture allows to

significantly increase the energy density of the burning material due to increase of the amount of kerosene required for complete burnout in the unit volume.

- (2) It has been shown that detonability of kerosene – hydrogen peroxide blends increases significantly with the content of H<sub>2</sub>O<sub>2</sub>. In terms of the critical initiation energy, the kerosene–air mixtures with 5% and 20% of hydrogen peroxide were shown to be equivalent to stoichiometric ethylene–air and hydrogen–air mixtures, respectively.
- (3) Detonation parameters (velocity  $D_0$ , temperature and pressure) of kerosene–H<sub>2</sub>O<sub>2</sub>–air mixtures were shown to be almost independent of the molar fraction of H<sub>2</sub>O<sub>2</sub>, that is important for performance stability of advanced propulsion systems.
- (4) It has been found that addition of H<sub>2</sub>O<sub>2</sub> vapor to the hydrocarbon–air mixture results in increase of the specific impulse  $I_{sp}$ . This effect becomes apparent at molar concentrations of H<sub>2</sub>O<sub>2</sub> exceeding 10%.

## 3. Combustion Chemistry

To study the behavior of kerosene – hydrogen peroxide blends there is a need in kinetic mechanisms of their mutual oxidation. During previous studies [9, 10], the overall reaction mechanism of hydrocarbon fuel oxidation with regard for addition of H<sub>2</sub>O<sub>2</sub> aimed at ignition promotion were developed and verified.

To verify the applicability of the reaction mechanisms to modeling combustion of fuel blends containing considerable amounts of H<sub>2</sub>O<sub>2</sub>, a set of calculations was made for laminar flame propagation in gaseous mixtures containing H<sub>2</sub>O<sub>2</sub> and N<sub>2</sub>. As a

reference, a detailed reaction mechanism of H<sub>2</sub>O<sub>2</sub> decomposition was used. A reasonable agreement of the predicted results based on the overall and detailed reaction mechanisms was obtained.

The overall reaction mechanism for gaseous mixtures containing a hydrocarbon fuel, H<sub>2</sub>O<sub>2</sub> and air is presented in Table 1. The mechanism includes soot, NO and CO formation chemistry.

#### 4. Mathematical Model of Droplet Combustion

The mathematical model considers a single-component liquid droplet in the unconfined initially quiescent gaseous atmosphere. The droplet size is allowed to vary in time due to thermal expansion and liquid gasification processes. Droplet surface is treated as the moving boundary. In general, all physical properties of liquid and gas are pressure and temperature dependent. The constant-pressure approximation with independent diffusion of species in gas phase has been adopted. The set of governing equations includes full equations of thermal conductivity in both phases, continuity and species conservation equations in a gas phase, and the ideal equation of state for gaseous species. Radiation heat loss has been also taken into account.

Two types of droplet ignition procedures were used: (1) ignition by adopting a time-varying activation energy of a rate-controlling gas-phase reaction of hydrocarbon decomposition, and (2) ignition by making a provision of an ignition kernel — a narrow high-temperature zone occupied by combustion products. The behavior of a droplet was found to be fairly independent of the ignition procedure.

### 5. Combustion of a Single Droplet in Air

#### 5.1 Hydrocarbon Droplet

As reference hydrocarbons, *n*-tetradecane and *n*-heptane were considered. Figure 1 shows the comparison of predicted  $d^2 - t$ -curves for droplets of initial diameter 30  $\mu\text{m}$ . Obviously, *n*-heptane droplet exhibits higher combustion rate (1.2 mm<sup>2</sup>/s) than *n*-tetradecane droplet (0.95 mm<sup>2</sup>/s). The combustion constant  $K_{comb}$  was found to decrease with pressure and with droplet size.

#### 5.2 Hydrogen Peroxide Droplet

Figure 2 shows the predicted histories of the radius of a H<sub>2</sub>O<sub>2</sub> droplet of initial diameter 50  $\mu\text{m}$  at pressure  $p_0 = 5, 10, 20$  and 50 bar. The ambient air temperature is  $T_0 = 1000$  K. Initially, the temperature of the droplet is 300 K and no H<sub>2</sub>O<sub>2</sub> vapor is present in the ambient air.

With pressure increasing, the droplet lifetime decreases and the rate of droplet surface regression increases, that is different from the behavior of hydrocarbon droplets. At low pressure, the droplet lifetime exceeds 10 ms and the highest attained combustion temperature is 1060 K. Increase in pressure to 10 bar results in shortening the droplet lifetime to 10 ms and increase in the combustion temperature to 1400 K. Further increase in pressure to 20 and 50 bar results in a decrease of the droplet lifetime to 8 and 7 ms and in increase in the combustion temperature to 1700 K and 1800 K, respectively. Examining the  $d^2(t)$  plot for the H<sub>2</sub>O<sub>2</sub> droplet at  $T_0 = 1000$  K and  $p_0 = 50$  bar results in the following. Most of the lifetime the droplet evaporates at low rate ( $K_{evap} \approx 0.04$  mm<sup>2</sup>/s). After ignition of H<sub>2</sub>O<sub>2</sub> vapor accumulated in the vicinity of the droplet, the rate of surface regression increases by two orders of magnitude and becomes very large ( $K_{comb} \approx 3.0$  mm<sup>2</sup>/s). Note that droplets of hydrocarbons exhibit  $K_{comb} \approx 0.6-1.5$  mm<sup>2</sup>/s depending on droplet size and pressure.

The effect of droplet diameter on combustion intensity of a single H<sub>2</sub>O<sub>2</sub> droplet is illustrated by Table 2. Small droplets have shorter lifetime and exhibit smaller combustion rates. A droplet of  $d_0 = 10$   $\mu\text{m}$  has low combustion temperatures (less than 1020 K) due to relatively low concentration of H<sub>2</sub>O<sub>2</sub> vapor in droplet vicinity. The maximum combustion temperature at  $d_0 = 20$   $\mu\text{m}$  is 1340 K. With increasing the initial droplet size to 30 and 50  $\mu\text{m}$  the maximum combustion temperature grows to 1600 K and 1800 K, respectively.

### 6. Hybrid Combustion

The term ‘hybrid combustion’ adopted here means (1) combustion of a hydrocarbon droplet in air mixed with H<sub>2</sub>O<sub>2</sub> vapor, (2) combustion of a H<sub>2</sub>O<sub>2</sub> droplet in air mixed with hydrocarbon vapor, or (3) combustion of a hydrocarbon droplet in hot exhaust gas mixed with H<sub>2</sub>O<sub>2</sub> vapor. Such a study is expected to provide a valuable information on the reactivity of the two liquid fuels injected simultaneously into a combustion chamber.

#### 6.1 Hydrocarbon droplet in air–H<sub>2</sub>O<sub>2</sub> vapor mixture

Figure 3 shows the histories of the *n*-heptane droplet radius depending on the volume fraction of H<sub>2</sub>O<sub>2</sub> vapor in air. In all the cases, the initial droplet diameter is 50  $\mu\text{m}$ , initial droplet temperature 300 K, and ambient pressure  $p_0 = 20$  bar.

It follows from Fig. 3 that addition of H<sub>2</sub>O<sub>2</sub> vapor to the gas phase results in a significant transformation of *n*-heptane droplet behavior. With addition of 5% and 10% (vol.) of H<sub>2</sub>O<sub>2</sub> vapor, the lifetime of the droplet decreases from 6 ms to 2 ms and 1 ms, respectively. Moreover, under the specified conditions, the *n*-heptane droplet simply evaporates rather than burns in pure air.

Figure 4 shows the example of the computed temperature histories during droplet combustion. Droplet ignition is promoted by the localized ignition of H<sub>2</sub>O<sub>2</sub> vapor. Ignition of the vapor results in subsequent laminar flame propagation in the gas phase outwards of the droplet surface. The flame has an unusual double-front structure. The forward part of the flame propagates through H<sub>2</sub>O<sub>2</sub> vapor. Oxygen formed due to decomposition of H<sub>2</sub>O<sub>2</sub> is then consumed in oxidation reactions of *n*-heptane vapor. The temperature rise in the forward flame is about 400 K. In the subsequent flame, temperature increases by about 2000 K. The apparent flame velocity is 70 to 100 cm/s. The flame propagates in H<sub>2</sub>O<sub>2</sub> vapor that gradually decomposes in the bulk. This is indicated in Fig. 4 by the growing level of temperature in front of the flame.

### 6.2 H<sub>2</sub>O<sub>2</sub> droplet in air–hydrocarbon vapor mixture

Figure 5 shows the histories of the H<sub>2</sub>O<sub>2</sub> droplet size depending on the volume fraction of *n*-heptane vapor in air. It follows from Fig. 5 that addition of *n*-heptane to the gas phase results in a significant transformation of H<sub>2</sub>O<sub>2</sub> droplet behavior. With addition of 0.2% and 0.5% (vol.) of *n*-heptane vapor, the lifetime of the droplet decreases to 5 ms and 3 ms, respectively, that is much less than the lifetime of the H<sub>2</sub>O<sub>2</sub> droplet in pure air (about 50 ms). Note that under the specified conditions, the H<sub>2</sub>O<sub>2</sub> droplet evaporates rather than burns.

As an example of temperature histories, Fig. 6 indicates violent ignition and combustion of the H<sub>2</sub>O<sub>2</sub> droplet in air with 0.5%(vol.) *n*-heptane vapor. Combustion of the H<sub>2</sub>O<sub>2</sub> droplet is characterized by a relatively low combustion temperature (about 1600 K). In Fig. 6, there exists a gas-phase flame propagating outwards of the droplet at the velocity of 30–40 cm/s.

### 6.3 Hydrocarbon droplet in exhaust gas–H<sub>2</sub>O<sub>2</sub> vapor mixture

Figures 7 and 8 show the development of the temperature field around the *n*-heptane droplet placed initially into the atmosphere of hot combustion products and H<sub>2</sub>O<sub>2</sub> vapor. In both cases, the initial atmosphere

does not contain free oxygen and is composed of CO<sub>2</sub>, CO, H<sub>2</sub>O, H<sub>2</sub>, H<sub>2</sub>O<sub>2</sub> and N<sub>2</sub>.

Figure 7 is plotted for the test case when the initial molar concentration of H<sub>2</sub>O<sub>2</sub> is 20%. Auto-ignition occurs in less than 10 μm (!) after starting the calculation. This happens due to extremely fast decomposition of H<sub>2</sub>O<sub>2</sub> resulting in the formation of free oxygen that then reacts with hydrocarbon vapor. In the following, a hybrid flame is established in the system. The flame front propagates through the H<sub>2</sub>O<sub>2</sub> vapor outwards of the droplet. Free oxygen produced in this flame is consumed by combustion reactions of *n*-heptane vapor delivered by the droplet evaporation process.

Decrease in the initial concentration of H<sub>2</sub>O<sub>2</sub> from 20% (Fig. 7) to 10% (Fig. 8) results in a longer development of the hydrocarbon flame. The temperature rise in Fig. 8 is mainly due to combustion of H<sub>2</sub>O<sub>2</sub>.

A detailed study of such hybrid systems is continued. The objective of this study is to understand the underlying physics and chemistry of the encountered phenomena in order to elaborate the measures to control combustion and detonation of fuel blends.

## 7. Conclusion

In addition to accomplishments listed in Section 2, the following findings are to be mentioned:

- (1) Droplets of H<sub>2</sub>O<sub>2</sub> burn with a considerable temperature rise only at elevated pressures (> 5 bar) and at relatively large droplet size (> 30 μm). Combustion of fine H<sub>2</sub>O<sub>2</sub> droplets at atmospheric pressure shows low exothermicity.
- (2) Hybrid combustion of hydrocarbon fuel and H<sub>2</sub>O<sub>2</sub> shows a great variety of phenomena. Three modes of hybrid combustion have been studied, namely, (1) combustion of a hydrocarbon droplet in air mixed with H<sub>2</sub>O<sub>2</sub> vapor, (2) combustion of a H<sub>2</sub>O<sub>2</sub> droplet in air mixed with hydrocarbon vapor, and (3) combustion of a hydrocarbon droplet in hot exhaust gas (with no free oxygen) mixed with H<sub>2</sub>O<sub>2</sub> vapor. Such a study provides a valuable information on the reactivity of the two liquid fuels injected simultaneously into a combustion chamber. It has been proved, that hybrid combustion is much more efficient than combustion of single components in air.

The results will be used for elaborating improved strategies of active and passive control of combustion and detonation in advanced propulsion engines.

## References

- <sup>1</sup>Williams, W. F., Satterfield, C. N., Isbin, H. S. 1952. *J. Am. Rocket Soc.* 22:70.
- <sup>2</sup>Schumb, W. C., Satterfield, C. N., Wentworth, R. L. 1955. *Hydrogen peroxide*. N.Y.: Reinhold Publ. Corp., London: Chapman & Hall.
- <sup>3</sup>Seryshev, G. A. 1984. *Chemistry and technology of hydrogen peroxide*. Leningrad: Chemistry Publ.
- <sup>4</sup>Frolov, S. M., Basevich, V. Ya. 1999. "Application of fuel blends for active detonation control in a pulsed detonation engine," AIAA Paper A99-34130. Presented at the 14<sup>th</sup> ISOABE. Florence, Italy (ISABE 99-7129).
- <sup>5</sup>Frolov, S. M., Basevich, V. Ya. 1999. "The use of fuel blends and distributed injection for active detonability control in a PDE," Presented at the 17<sup>th</sup> ICDERS. Heidelberg, Germany.
- <sup>6</sup>Frolov, S. M., Basevich, V. Ya., Vasil'ev, A. A. 2000. "Evaluation of fuel blend composition for PDE applications," In: *Control of detonation processes*. Eds. G. D. Roy, S. M. Frolov, D. W. Netzer, and A. A. Borisov. Moscow: Elex-KM Publ.
- <sup>7</sup>Frolov, S. M., Basevich, V. Ya., Vasil'ev, A. A. 2000. "Detonation control by in-situ blending of liquid fuels," In: *Detonation and high-speed deflagration: Fundamentals to control*. Eds. G. D. Roy, S. M. Frolov, D. W. Netzer, and A. A. Borisov. Moscow: Elex-KM Publ.
- <sup>8</sup>Gueret, C., Cathonnet, M., Boettner, J. C., Gaillard, F. 1990. "Experimental study and modeling of kerosene oxidation in a jet-stirred flow reactor," *23<sup>rd</sup> Symposium (International) on Combustion Proceedings*. Pittsburgh, PA: The Combustion Inst. 211.
- <sup>9</sup>Frolov, S. M., Basevich, V. Ya., Belyaev, A. A., et al. 1997. "Study of turbulent flame stabilization and combustion control in subsonic and supersonic combustors by a joint velocity – scalar PDF method," *10<sup>th</sup> ONR Propulsion Meeting Proceedings*, Monterey: Naval Postgraduate School. 38–42.
- <sup>10</sup>Frolov, S. M., Basevich, V. Ya., Neuhaus, M. G., et al. 1996. "Application of a coupled finite volume – joint velocity – scalar PDF method for modeling turbulent combustion in a simple combustor," *9<sup>th</sup> ONR Propulsion Meeting Proceedings*. Washington, DC: Naval Research Laboratory. 305–317.

**Table 1:** Overall reaction mechanism of hydrocarbon–H<sub>2</sub>O<sub>2</sub> system

N	Reaction	H, kcal/mol	Forward			Reverse		
			A, mol, l, s	n	E, kcal/mol	A, mol, l, s	n	E, kcal/mol
1 <sup>a</sup>	$C_nH_{2n+2} + (n + 0.5)O_2 = nCO + (n + 1)H_2O$	614	$7.0 \cdot 10^{14}$	0.0	50.0			
2	$H_2 + H_2 + O_2 = H_2O + H_2O$	114	$7.0 \cdot 10^{13}$	0.0	21.0			
3	$CO + CO + O_2 = CO_2 + CO_2$	134	$8.5 \cdot 10^{12}$	0.0	21.0			
4	$H_2O + CO = H_2 + CO_2$	10	$1.0 \cdot 10^{12}$	0.0	41.5	$7.0 \cdot 10^{13}$	0.0	49.1
5 <sup>b</sup>	$R + R + M = H_2O + M$	118	$9.5 \cdot 10^{12}$	-1.0	0.0	$7.0 \cdot 10^{13}$	-2.0	120.0
6	$R + H_2 + O_2 = R + R + R + 0.5O_2$	-4	$4.5 \cdot 10^{14}$	0.0	16.4			
7	$H_2O_2 = R + R + 0.5O_2$	-92	$5.0 \cdot 10^{15}$	0.0	50.0			
8	$O_2 + C_nH_{2n+2} + N_2 = C_nH_{2n+2} + NO + NO$	-43	$2.0 \cdot 10^{14}$	0.0	50.0			
9	$O_2 + N_2 = NO + NO$	-43	$1.7 \cdot 10^{17}$	-0.5	136.0	$7.0 \cdot 10^{13}$	-0.5	93.3
10 <sup>c</sup>	$C_nH_{2n+2} + C_nH_{2n+2} = 2nC + (2n + 2)H_2$	-2430	$4.0 \cdot 10^{12}$	0.0	50.0			
11	$C + C + O_2 = CO + CO$	394	$2.6 \cdot 10^{14}$	0.0	0.0			

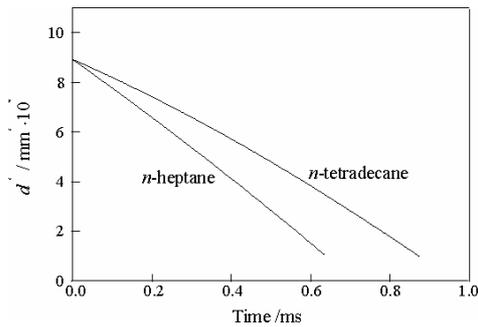
<sup>a</sup>Reaction rate  $W = k[C_nH(2n + 2)][O_2]$

<sup>b</sup>R is the conditional radical

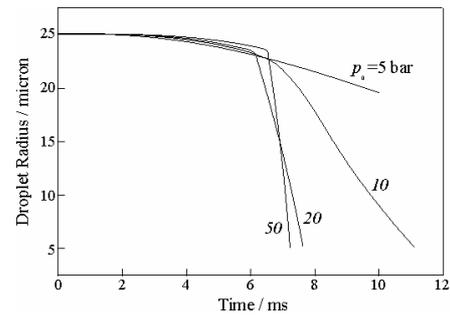
<sup>c</sup>C denotes soot

**Table 2:** Calculated values of the combustion constant  $K_{comb}$  for  $H_2O_2$  droplets in air at  $T_0 = 1000$  K,  $p_0 = 50$  bar and initial droplet temperature of 300 K

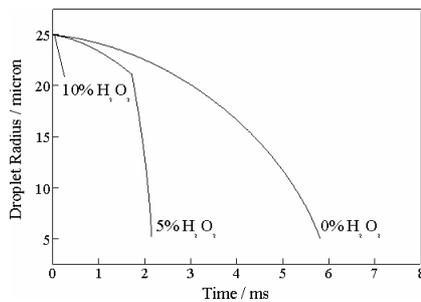
Droplet diameter, $\mu\text{m}$	10	20	30	50
Combustion constant $K_{comb}$ , $\text{mm}^2/\text{s}$	0.125	0.5	1.1	3.0



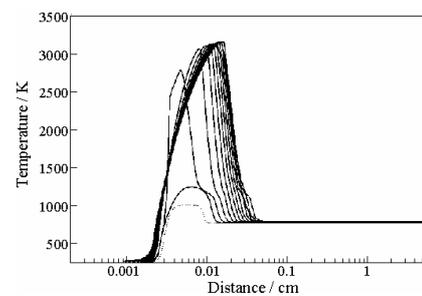
**Figure 1:** Comparison of predicted  $d^2 - t$  plots for the case of combustion of similar  $n$ -tetradecane and  $n$ -heptane droplets in air ( $d_0 = 30 \mu\text{m}$ ,  $p_0 = 10$  bar,  $T_0 = 1000$  K).



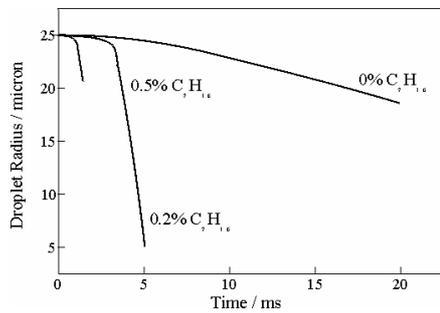
**Figure 2:** Predicted histories of  $H_2O_2$  droplet radius during combustion at different ambient pressure:  $p_0 = 5, 10, 20,$  and  $50$  bar. Initial droplet diameter  $50 \mu\text{m}$ , ambient temperature  $T_0 = 1000$  K.



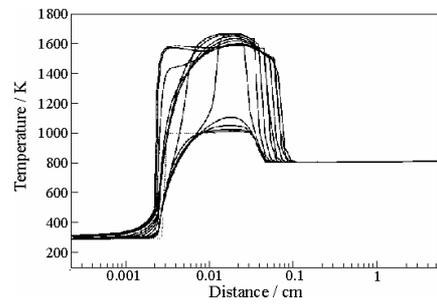
**Figure 3:** Predicted histories of  $n$ -heptane droplet radius during hybrid combustion in air mixed with various amounts of  $H_2O_2$  vapor (10% (vol.), 5% (vol.) and 0%) at pressure  $p_0 = 20$  bar. Droplet diameter  $50 \mu\text{m}$ , ambient temperature  $T_0 = 800$  K.



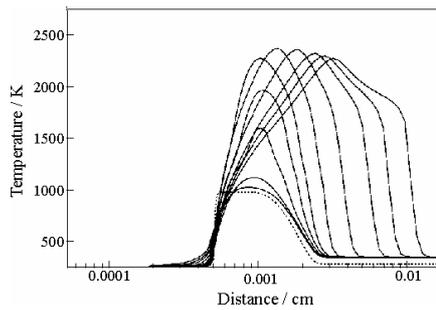
**Figure 4:** Temperature history for combustion of  $n$ -heptane droplet in air with addition of 10% (vol.)  $H_2O_2$  vapor. Droplet diameter  $50 \mu\text{m}$ , pressure  $p_0 = 20$  bar. Dotted line shows initial distribution of ambient temperature.



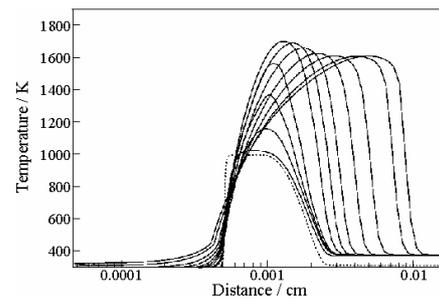
**Figure 5:** Predicted histories of  $\text{H}_2\text{O}_2$  droplet radius during hybrid combustion in air mixed with various amounts of  $n$ -heptane vapor (0.5% (vol.), 0.2% (vol.) and 0%) at pressure  $p_0 = 20$  bar. Initial droplet diameter  $50 \mu\text{m}$ , ambient temperature  $T_0 = 800$  K.



**Figure 6:** Temperature history for combustion of  $\text{H}_2\text{O}_2$  droplet in air with addition of 0.5% (vol.)  $n$ -heptane vapor. Initial droplet diameter  $50 \mu\text{m}$ , pressure  $p_0 = 20$  bar. Dotted line shows initial distribution of ambient temperature.



**Figure 7:** Development of the temperature field around an  $n$ -heptane droplet placed initially into the atmosphere of hot combustion products and  $\text{H}_2\text{O}_2$  vapor (20% (vol.)). Initial atmosphere does not contain free oxygen, droplet diameter  $10 \mu\text{m}$ , pressure  $p_0 = 20$  bar. Dotted line shows initial distribution of ambient temperature.



**Figure 8:** Development of the temperature field around an  $n$ -heptane droplet placed initially into the atmosphere of hot combustion products and  $\text{H}_2\text{O}_2$  vapor (10% (vol.)). Initial atmosphere does not contain free oxygen, droplet diameter  $10 \mu\text{m}$ , pressure  $p_0 = 20$  bar. Dotted line shows initial distribution of ambient temperature.